

# Pertechnetate immobilization with amorphous iron sulfide

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(Received September 12, 2007; accepted in revised form May 27, 2008)

*Technetium-99 / Iron sulfide / Pertechnetate immobilization*

**Summary.** The reduction of pertechnetate ( $\text{TcO}_4^-$ ) with freshly prepared amorphous iron sulfide was investigated. The amorphous iron sulfide ( $\text{FeS}$ ) was shown to have an elemental composition of  $\text{FeS}_{0.97}$  for all of the size fractions and a point of zero charge of  $\text{pH}_{\text{pzc}} = 7.4$ . Solubility studies of  $\text{FeS}$  in various buffers indicated that in the pH range 6.1–9.0, the concentrations of dissociated  $\text{Fe}^{2+}$  and  $\text{S}^{2-}$  were negligible. The reductive immobilization of  $\text{TcO}_4^-$  with  $\text{FeS}$  was shown to be accelerated by increasing ionic strength and strongly pH dependent. At pH values below the  $\text{pH}_{\text{pzc}}$ , the positively charged  $\text{FeS}$  surface reacted much faster with  $\text{TcO}_4^-$  and had higher immobilization yields relative to the negatively charged  $\text{FeS}$  surface at pH values above  $\text{pH}_{\text{pzc}}$ . The  $\text{TcO}_4^-$ - $\text{FeS}$  reaction is consistent with a surface mediated reaction through ligand exchange. The  $\text{TcO}_4^-$ - $\text{FeS}$  reductive immobilization reaction product was characterized by X-ray absorption near edge spectroscopy (XANES), extended X-ray absorption fine structure (EXAFS), Fourier transform infrared spectroscopy (FT-IR), and energy dispersive X-ray spectroscopy (EDS) and found to be predominantly  $\text{TcO}_2$ . Studies on the reductive capacity of the  $\text{FeS}$  and the long term stability of the  $\text{TcO}_4^-$ - $\text{FeS}$  reaction product under both anaerobic and aerobic environments shows the potential utility of the *in situ* gaseous (hydrogen sulfide gas) immobilization technology in solidification of  $\text{TcO}_4^-$  by creating a  $\text{FeS}$  permeable reaction barrier in the vadose zone.

## Introduction

The Department of Energy Hanford Site in eastern Washington State is the largest nuclear waste storage site in the United States, with 54 million gallons of radioactive waste contained underground in storage tanks [1–3]. The first tank leak, reported in 1956, was a result of corrosion, with about 67 tanks believed to have leaked about 0.75–1.5 million gallons of radioactive waste into the soil, resulting in the contamination of the vadose zone [4].

Among the 46 radionuclides in the waste tanks [5], technetium-99 ( $\text{Tc-99}$ ) is of considerable interest due to the quantities present, its long half-life ( $t_{1/2} = 2.13 \times 10^5$  years), and its diverse chemistry [6–8]. Various remediation methods for technetium contamination in the vadose zone from tank leakage at the Hanford Site have been considered [9–14]. The gas-phase approach using hydrogen

sulfide ( $\text{H}_2\text{S}$ ) gas, which is specifically designed for vadose zone treatment, is attractive due to  $\text{Tc-99}$  contaminated soil. The relatively easy introduction of the  $\text{H}_2\text{S}$  gas to the vadose zone, the control of  $\text{H}_2\text{S}$  delivery, and the efficient removal of  $\text{H}_2\text{S}$  gas after completion of the treatment all add to the potential utility of the *in situ*  $\text{H}_2\text{S}$  gaseous remediation method to both laboratory and real field applications [15–17].

The concentration of  $\text{TcO}_4^-$  in the tanks was at the  $10^{-5}$  M level, indicating the  $\text{TcO}_4^-$  concentration in the vadose zone would be lower than this. Once the  $\text{H}_2\text{S}$  gas, in large excess, is introduced into the vadose zone, the fraction of  $\text{H}_2\text{S}$  that reacts with  $\text{TcO}_4^-$  and the rate of oxidation of  $\text{H}_2\text{S}$  in the gas phase would be insignificant [2, 18]. As a result, the main pathway for excess  $\text{H}_2\text{S}$  consumption in the vadose zone would involve reactions with minerals.

Iron oxides are the major constituents of the soil in the vadose zone [19, 20] and they have been reported to effectively remove  $\text{H}_2\text{S}$  from the gas stream through a gas–solid reaction, to a theoretical maximum of 0.6 g  $\text{H}_2\text{S}$ /g Fe-oxide(s) [21]. This indicates that significant amounts of  $\text{H}_2\text{S}$  would be consumed by iron oxides present in the vadose zone during *in situ* gaseous immobilization to generate significant quantities of iron sulfide ( $\text{FeS}$ ) [22, 23].  $\text{FeS}$  might also be generated from dissimilatory sulfate reduction by bacteria present in the soil [24, 25] with no difference in the  $\text{FeS}$  product [26, 27].

Amorphous  $\text{FeS}$  is a highly reactive phase and has been widely used to reduce mobile non-radioactive metal oxyanions to insoluble species [28–30]. The interaction between iron sulfide and  $\text{TcO}_4^-$  showed that  $\text{TcO}_4^-$  in aqueous solution could be effectively reduced and coprecipitated with  $\text{FeS}$  [31–34], with a  $\text{TcS}_2$ -like product identified by X-ray absorption spectroscopy [35–37]. Further studies on the re-oxidation of the  $\text{FeS}$  host with aging showed that rather than being oxidized back to  $\text{TcO}_4^-$ , a  $\text{TcO}_2$ -like phase formed, indicating that long term immobilization might be achieved [36, 37]. Based on these results, it may be possible to inject  $\text{H}_2\text{S}$  gas into the vadose zone to reduce the iron oxides to  $\text{FeS}$ , creating a permeable reactive barrier of  $\text{FeS}$  for preventing the migration of  $\text{TcO}_4^-$ . However, the  $\text{FeS}$ - $\text{TcO}_4^-$  reaction is not well understood regarding the stoichiometry of the reaction, factors influencing the reaction, the reaction capacity, or the product characterization. The objectives of this study were to (1) study the basic chemistry between  $\text{FeS}$  and  $\text{TcO}_4^-$  in aqueous solution under anaer-

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